

ASPHALT ADDITIVE MIXING APPARATUS AND METHODS

RELATED APPLICATIONS

5 This application claims the benefit of the filing date under 35 U.S.C. §119 of
Great Britain Application No. 0016442.6, filed July 4, 2000, which is hereby
incorporated by reference in its entirety.

FIELD OF THE INVENTION

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The present invention relates to the production of high quality pavement. In particular, the present invention relates to an apparatus and methods suitable for incorporating pelletised additives into thin surface dressings.

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BACKGROUND OF THE INVENTION

Stone Mastic Asphalt (SMA), an example of a thin surface dressing, was developed in the early 1970s in Germany (originally to resist the wear of studded tyres) where to date, over 250 million square metres of highway have been paved with this product. The successful production of SMA is typically made possible with the use of stabilising additives in the form of highly specialised cellulose fibres. These prevent excessive drainage of the asphalt binding agent (bitumen).

The advantages of thin surface dressings over conventional road surface applications are now well recognised and its use is increasing at a steady pace. For example, due to its excellent characteristics and performance, SMA has been adopted in many countries, including the Netherlands, France, Switzerland, UK, Norway, Finland, Sweden, Denmark, Turkey, Greece, Poland, Japan, Israel and the USA.

Asphalt production plants which manufacture blends of aggregate and bitumen for use in the production of thin surface dressings, were not designed with these new products in mind. Such plants consist of large storage vessels holding bulk raw materials, such as aggregate and bitumen, which are then conveyed to a central elevated mixing box for blending. The asphalt mixing box typically has a height similar to that of a three or four story building. The raw materials are typically mixed in a ratio of 1 tonne of aggregate to 200 kg of fillers and binders, the latter typically comprising 70-100 kg of bitumen. Blending takes place at an elevated temperature of typically 170°C. However, the industry is moving towards production of technically more sophisticated thin surface dressings that require the incorporation of multiple additives. In contrast to the relatively large proportion of bitumen in a finished asphalt product, these further additives are incorporated in relatively small amounts, such as 3 kg of fibre, 10 kg of pigment and 5 kg of a polymer modifier per tonne of aggregate.

Accordingly, these new products are manufactured today either by manual addition of the multiple additives into the asphalt mixing box or by means of a supply system as shown in Fig. 1.

The additive supply system shown in Fig. 1 comprises components and operates as follows. A bulk silo 10 for storing an additive in pelletised form is filled by means of a filler pipe 12. Additive can be added to the bulk silo 10 by being blown up filler pipe 12. A safety ladder 14 enclosed by safety rails 16 provides access to a hinged roof hatch 18 at the top of bulk silo 10. A high level probe 20 located at the top of bulk silo 10 indicates when the silo is full. Gas is exhausted down exhaust pipe 22, to which a cyclone dust collector 24 is fitted. The bulk silo 10 is emptied by agitation of its contents at low level using rotary electric vibrators 26. A level probe 28 and an emergency low level probe 30 respectively indicate when the bulk silo 10 is nearly or completely empty. Additive leaving the silo is conveyed by a supply auger 32 to the asphalt mixing box. The supply auger may be provided with

a calibration or sampling point 34 and an acoustic flow detection sensor 36. The
auger 32 is driven by a drive unit 38 which draws additive to outlet 40 and into the
asphalt mixing box. The elevated asphalt mixing box is accordingly fed with
additive from the bulk silo 10 from above. The quantity of additive added to each
5 batch of asphalt is controlled simply by the run duration time of drive unit 38.

SUMMARY OF THE INVENTION

The inventors have appreciated that both the manual addition of additives and
10 the Fig. 1 supply system may have disadvantages as follows.

Manual addition of additives into the mixing box creates health and safety
hazards for operators, as the additives can be dusty and of a dangerous nature.
Manual addition also has a tendency to result in inconsistency in the blending
15 process, accidental losses and inconsistent end products.

On the other hand, the additive supply system shown in Fig. 1, which reduces
these hazards, is only designed to incorporate a single additive volumetrically into
the asphalt mixing box.
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In addition, asphalt production plants are often sited in restricted areas where
storage space is limited. The current design of these plants requires that storage
vessels for additives, such as that shown in Fig. 1, are located significant distances
from the asphalt mixing box. This is because supply auger 32 shown in Fig. 1 cannot
25 be oriented at an angle greater than about 45° to the horizontal, otherwise additive
pellets drop back down the auger under gravity and the flow of additive from silo 10
to the asphalt mixing box is impeded. Accordingly, storage facilities for each new
additive required would similarly need to be sited at an appreciable distance from the
asphalt mixing box and augered in. If the asphalt product in question requires a
30 number of additives, storage systems as shown in Fig. 1 would need to be replicated

in said receptacle into a blend; and transferring said blend from said receptacle for delivery to an asphalt mixing box.

In a third aspect, the present invention further provides an apparatus for
5 delivering additives for incorporation in an asphalt to an asphalt mixing box, said
apparatus comprising: a receptacle constructed and arranged to receive said additives,
said receptacle having an input for said additives locatable at a level substantially
lower than an input for said additives to said asphalt mixing box; a mixer adapted to
10 mix said additives and prepare a blend; a transfer pipe connected between an output
of said receptacle to the input of said asphalt mixing box; and a pneumatic pressure
source connected to said transfer pipe that conveys said blend along said transfer pipe
from near the output of said receptacle to the input of said asphalt mixing box.

In a fourth aspect, the present invention further provides a method of
15 delivering additives for incorporation in an asphalt to an asphalt mixing box, said
method comprising: supplying said additives to a receptacle for preparing a blend of
said additives at a level substantially lower than an input for said additives to said
asphalt mixing box; and pneumatically conveying a blend of additives output of said
receptacle to the input of said asphalt mixing box.

In one illustrative embodiment, an apparatus according to the third aspect of
the invention uses an apparatus according to the first aspect of the invention as means
for preparing a blend of said additives. In other words, an apparatus according to the
first aspect of the invention preferably uses an apparatus according to the third aspect
25 of the invention as means for delivering said blend to an asphalt mixing box.
Likewise, a method according to the fourth aspect of the invention further comprises,
after said supplying step and before said conveying step, blending said additives by a
method according to the second aspect of the invention. In other words, a method
according to the second aspect of the invention preferably further comprises a

method of delivering said additives to an asphalt mixing box according to the fourth aspect of the invention.

In another illustrative embodiment, the apparatus according to the first aspect
5 of the invention further comprises a control system having an input from a weighing means, such as the scale, and control outputs to an inlet of said receptacle and to said mixer and said transport system, said control system being programmable to regulate receipt of said additives through said receptacle inlet based on gravimetric amounts of additives measured by said weighing means until a desired total amount of said
10 additives in desired proportions thereof is achieved, and to operate said mixer and said transport system sequentially thereafter.

The features of an apparatus according to the first aspect of the invention and of a method according to the second aspect of the invention may give improved
15 performance, consistency and range of end products after incorporation of the additives into an asphalt. Accordingly, these aspects of the invention provide an effective manner of creating a wide palette of easily reproducible coloured thin surface dressings, such as those required for speciality applications, by blending pelletised colour pigments to create a consistent range of graded colours. The
20 improved accuracy of desired proportions of additives and thorough pre-blending that may be achieved by these aspects of the invention prior to their incorporation into an asphalt give improved performance characteristics due to the improved uniformity of dispersion of the additives in question through the asphalt when laid as a pavement.

25 The third and fourth aspects of the invention may provide advantages in the siting and distribution of additive storage vessels around an asphalt mixing box. Since the means for preparing a blend of said additives has an input for said additives locatable at a level substantially lower than an input for said additives to said asphalt
30 mixing box, additive storage vessels may be located very close to said blending

means. This is because augers delivering additives from said additive storage vessels need only cover a small horizontal distance in order to lift additives from the respective storage vessels to a height sufficient to be input to the blending means in comparison to the much larger horizontal distance that would otherwise be required to lift additives from the respective storage vessels to the top of an asphalt mixing box. On the other hand, since a pneumatic pressure source is used to convey a blend of additives from an output of said blending means to an input of said asphalt mixing box, the transfer pipe connecting the output of the blending means to the input of the asphalt mixing box may include a vertical portion, which would not be achievable with an auger. For this reason, the blending means may be located very close to the asphalt mixing box. A large number of additive storage vessels may therefore be sited in close proximity to an asphalt mixing box, which has previously been impossible. The pneumatic pressure source may either be a blower or a vacuum pump.

Preferably, although not necessarily, the additives are blended and delivered to the asphalt mixing box in pelletised form. This may aid both the blending and the delivery procedures.

BRIEF DESCRIPTION OF THE DRAWINGS

Further features and advantages of the present invention will be better understood by reference to the following detailed description giving in association with the accompanying drawings, in which:

Fig. 1 is a side elevational view of a conventional supply system for providing an additive to an asphalt mixing box;

Fig. 2 is a side elevational view of an additive mixing apparatus according to an embodiment of the invention, shown in situ with a plurality of additive storage vessels;

5 Fig. 3 is a plan view of the arrangement shown in Fig. 2;

Fig. 4 is a side elevational view of an embodiment of an additive mixing apparatus shown in situ with a single additive storage vessel;

10 Fig. 5 is a plan view of the arrangement shown in Fig. 4;

Fig. 6 is a close-up side elevational view of the Fig. 4 additive mixing apparatus, showing the internal components thereof;

15 Fig. 7A is a side elevational view of the exterior of the additive mixing apparatus;

Fig. 7B is a plan view of the exterior of the additive mixing apparatus shown in Fig. 7A;

20 Fig. 7C is a front elevational view of the exterior of the additive mixing apparatus shown in Fig. 7A; and

Fig. 7D is a rear elevational view of the exterior of the additive mixing apparatus shown in Fig. 7A.

DETAILED DESCRIPTION

Referring firstly to Fig. 2, an embodiment of an additive mixing apparatus according to the invention, represented generally by reference numeral 200, is shown

in association with a plurality of additive storage vessels. The additive storage vessels may comprise one or more bulk silos 10 of the type also shown in Fig. 1 and/or one or more cari silos 100. Whereas bulk silos 10 are permanently sited, a cari silo may be removed and replaced using a fork-lift truck. Apparatus 200 is connected to each of the additive storage vessels associated therewith by an independent centreless auger for each respective storage vessel as indicated by reference numerals 32 in Fig.3. Each additive may be stored in pelletised form in a respective silo of appropriate size defined by the expected addition rate of the additive in question to the thin surface dressings to be prepared. As shown in Fig. 2, apparatus 200 is provided with a transfer pipe 210, by means of which blended pelletised additives are transferred by a positive pressure pneumatic conveying system to an elevated asphalt mixing box (not shown), where they are combined with the bulk components such as aggregate and bitumen.

Fig. 4 shows apparatus 200 in association with a single cari silo 100. Apparatus 200 comprises a material reception hopper 202 which enables precise, reproducible batch quantities of pelletised additives to be weighed in controlled conditions using a scale, which may include one or more high-accuracy load cells 214 (shown later in Fig. 6), other force or pressure transducers, a balance-type mechanism, a spring or other member whose deformation is indicative of the weight of the additives, or any other suitable weighing apparatus or weighing means. Apparatus 200 further comprises a transport system that transports the additives from the hopper 202 for delivery to an asphalt mixing box and may include one or more of a blower 204, a pneumatic slide valve 206, a rotary valve 208, and a silencer 212, all of which are described in greater detail below in association with Fig. 6. That is, the transport system may include only the rotary valve 208 or other similar apparatus that delivers material from the hopper 202, or may include the rotary valve 208, the slide valve 206, and the silencer 212. Of course, in some embodiments, the transport system may be arranged to include or operate in cooperation with other elements than those shown in Fig. 6, such as auger-type transport systems, conveyors, etc.

Cari silo 100 is provided with a hinged top hatch 118 and visual level indicators 128, and is mounted on the weatherproof slide 104 of a base unit 106. Base unit 106 further comprises a fixed ladder 114 with safety rails 116, fork lift channels 102 to permit removal of cari silo 100 from base unit 106, and an auger pick-up unit 108 for connection of cari silo 100 to supply auger 32. Auger pick-up unit 108 is designed to minimise losses of additive by use of a valve at the base of the cari silo, which seals the silo when disconnected from auger 32.

Fig. 5 shows the same arrangement as above, in which the cari silo and apparatus according to this embodiment are again represented by reference numerals 100 and 200, respectively.

A close-up side elevational view of the apparatus 200 is shown in Fig. 6, which reveals the internal components of apparatus 200. In this embodiment, apparatus 200 comprises components and operates as follows. Material reception hopper 202, which may have a capacity of 200 litres, receives pelletised additives from one or more supply augers 32. A scale, in this embodiment one or more load cells 214 which are tared to account for the weight of material reception hopper 202 when empty, permit gravimetric addition of pelletised additives to hopper 202 in desired proportions. In the present embodiment, load cell 214 has a capacity of 250 kg and is provided with optional anti-vibration, anti-shock loading mounting pads. In an alternative embodiment not shown in Fig. 6, material reception hopper 202 may instead be suspended from three load cells each having a capacity of 100 kg, which themselves are suspended from the main body of apparatus 200. Other scale arrangements will occur to those of skill in the art, such as arrangements in which additives are weighed before being deposited in the hopper 202. Sequential addition of additives of known weight from their respective storage vessels gives an extremely flexible system. With these embodiments, a weighing accuracy of +/- 0.5% can be achieved. This control eliminates problems with over-dosage and

accidental spillage of the pelletised additives, which are expensive. Following addition of pelletised additives in desired proportions to the hopper 202 as determined by means of load cell 214, the contents of hopper 202 are mixed by a mixer, which in this embodiment includes a vertical auger centrally located in the hopper 202, although the mixer may include other elements such as paddles, a vibratory mixing arrangement, or other mixing means to mix the additives into a blend (not shown in Fig. 6). The blend of additives created need not be a perfect mixture, instead any suitable mixing of the additives, whether in pelletised, powder or other form, may constitute a blend.

Once mixed, the pelletised additives are transferred from material reception hopper 202 via a rotary valve 208 located at the bottom of the hopper. From hopper 202, the mixture of pelletised additives is directed by rotary valve 208 to transfer pipe 210. Rotary valve 208 is driven by a motor having a power of typically 0.75kW to provide a rotor speed of from 50 to 70 rpm. The pelletised additives may then be forced along transfer pipe 210 by air from blower 204. The rotary valve 208 may control the flow of material along transfer pipe 210 to give a constant rate of flow therein. The rate of rotation of rotary valve 208 may be linked to the operation of blower 204. This is sequenced by means of a control timer provided on a main control panel of apparatus 200 (not shown in Fig. 6). In two preferred embodiments, blower 204 may have a power of 5.5kW and operate at 2900 rpm or 7.5kW and operate at 3000 rpm, providing a conveying rate of the pelletised additives along transfer pipe 210 of between 12 and 24 m³ per hour, according to throughput requirements. Approximate throughput rates, expressed in tonnes per hour, are shown in Table I.

TABLE I

Horizontal length of transfer pipe 210	Vertical length of transfer pipe 210	No. of 90° bends in transfer pipe 210	Approx. throughput	
			5.5kW blower	7.5kW blower
5m	7m	2	11 t/h	14 t/h
5m	10m	3	9 t/h	11 t/h
10m	10m	2	9 t/h	12 t/h
10m	15m	3	7 t/h	9 t/h
15m	15m	4	6 t/h	8 t/h
15m	20m	5	5 t/h	6 t/h

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In order to adjust the rate of flow of air output by blower 204 to transfer pipe 210, apparatus 200 may include a slide valve 206. Slide valve 206 is pneumatically operated to vary the air output from blower 204 to transfer pipe 210 according to requirements. Air output by blower 204 can be diverted from transfer pipe 210 by slide valve 206 to an exhaust outlet. This permits the blower to be kept running at a constant rate when the rate of flow of air from blower 204 to transfer pipe 210 needs to be varied according to requirements or even when no additives are to be propelled along transfer pipe 210 at all. Adjusting the rate of revolution of blower 204 or switching blower 204 on and off, both of which shorten its working lifetime, may thereby avoided, and may extend the working lifetime of the blower. A silencer 212 may be fitted to the exhaust from slide valve 206 for health and safety reasons.

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Figs. 7A to 7D show the exterior appearance of apparatus 200. The components shown in Fig. 6 and described above are contained within an enclosure,

which is preferably manufactured from Plastisol™ coated steel. The enclosure may be provided with removable access panels to permit servicing of the internal components of apparatus 200. Typical exterior dimensions of the enclosure are 2.4m in length by 1.3m in width by 1.9m in height.

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Apparatus 200 is very versatile because storage vessels for the pelletised additives, particularly if cavi silos 100 of the type shown in Fig. 4, are interchangeable, allowing different pelletised additives to be combined and mixed in desired proportions. Pelletised fibres, colour pigment pellets, binders and polymers may therefore all be added to an asphalt mixing box by means of the apparatus 200 in desired proportions and at the same time in a well pre-blended condition. As apparatus 200 is fully automated, the health and safety risks of manual handling of non-pelletised additives may be eliminated. Asphalt mixing cycle times may also be kept to a minimum by eliminating the need for dry mixing of non-pelletised additives prior to the wet mix process conducted in the main asphalt mixing box through pre-blending of pelletised additives by means of apparatus 200. This enables better additive dispersion in the asphalt product and consistent product density, through the use of pelletised additives.

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The above preferred embodiments have been described by way of example only and other embodiments of the present invention will be apparent to those skilled in the art from consideration of the detailed description given above and of the accompanying drawings. Thus any limitations on the present invention are to be found only in the claims set out below.